Characterization of Pd/γ -Alumina Catalysts Containing Ceria

J. Z. SHYU,¹ K. Otto,² W. L. H. Watkins, G. W. Graham, R. K. Belitz, AND H. S. GANDHI

Research Staff; Ford Motor Company, P.O. Box 2053, Dearborn, Michigan 48121

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The effects of adding $CeO₂$ to $Pd/A₂O₃$ as a catalyst modifier were investigated by X-ray photoelectron spectroscopy and X-ray diffraction. Catalytic effects were demonstrated by using propane oxidation as a model reaction. It was found that $CeO₂$ promotes oxidation of Pd to PdO both with and without alumina. High-temperature reduction $(\simeq 920^{\circ}C)$ and the presence of Pd are required for the total conversion to bulk CeAIO₃ from $CeO₂/Al₂O₃$. Pd also assists in the oxidation of bulk CeAIO₃ to CeO₂ at elevated temperatures. In ambient air, Pd facilitates surface oxidation of CeAIO₃ to CeO₂, whereas surface Pd acquires an oxidation state between Pd⁰ and PdO. On Pd/Al₂O₃ the propane oxidation rate is found to be lowered by $CeO₂$ if the oxygen concentration exceeds that of the stoichiometric ratio. \circ 1988 Academic Press, Inc.

1. INTRODUCTION

Ceria (CeO₂) has been widely applied as an additive in automotive catalysts because of its abilities to store oxygen $(1-4)$ and to improve dispersion of Pt $(3, 4-6)$ and Rh $(3, 4-6)$ 4). Reduction of ceria on alumina in H_2 involves at least two reactions, namely, formation of nonstoichiometric cerium oxides $(7-11)$ and cerium aluminate (CeAlO₃), depending on ceria loading $(10-12)$. The aluminate remains stable in air at $600-800^{\circ}$ C (10, 12). In a previous study, it was noted that in H_2 above 600°C dispersed ceria is completely transformed to $CeAlO₃$, while only partial conversion from ceria in the particulate phase to $CeAlO₃$ is observed even at 920°C (12). It was of interest to explore the effects of precious metals (PMs) on the formation of $CeAlO₃$ from ceria in the particulate phase resulting from PMceria interactions.

The purpose of this paper is to characterize chemical and structural changes due to interaction among Pd, ceria, and alumina by XPS (X-ray photoelectron spectroscopy) and XRD (X-ray diffraction) under oxidizing and reducing conditions. Catalytic changes resulting from this interaction are demonstrated by using propane (C_3H_8) oxidation as a model reaction. Implications of this work in automotive catalysis are discussed. A parallel study involving Pt on $CeO₂/Al₂O₃$ is presented in a companion paper.

2. EXPERIMENTAL SECTION

2.1. Materials

CeO₂, CeO₂/Al₂O₃, and CeAlO₃/Al₂O₃ were prepared by the methods described previously (12). Samples that contain Pd were prepared by impregnation of $CeO₂$, $CeO₂/Al₂O₃$, and $CeAlO₃/Al₂O₃$ with aqueous solutions of $Pd(NO₃)₂$. The alumina support was obtained from Degussa (alumina-C) and had an initial BET area of 100 \pm 20 m²/g.

2.2. Propane Oxidation Actiuity Measurements

Propane oxidation was studied with a flow reactor system equipped with a flame ionization detector (FID). The reactant mixture was composed of 1000 ppm C_3H_8 in N_2 with varying amounts of oxygen. The

^{&#}x27; Current address: Amoco Research Center. P.O. Box 400 —Building 600 . Naperville, II. 60566 .

² To whom correspondence should be addressed.

gas flow rate was set at \simeq 1500 ml/min. The catalyst weight was typically 0.2 g. All samples were reduced in 3% H₂ (in N₂) at 500° C for 3 h and then cooled to room temperature before introduction of the reactant mixture.

2.3. XPS and XRD Measurements

XPS data were recorded on a Surface Science Laboratory SSX-100 XPS spectrometer with monochromatized Al K_{α} Xrays. A 1000- μ m spot size and 100-eV analyzer pass energy were typical for the analysis. Sample charging during the measurement was compensated by an electron flood gun operated at approximately 2 eV. The electron takeoff angle was 35° from the sample surface. Reduction of catalyst samples was carried out in situ in flowing H_2 at $= 10$ ml/min in a reactor attachment (Physical Electronics) which can be operated at a maximum temperature of 600°C. Reduction of samples at higher temperatures was therefore carried out in a separate quartz reactor. These samples were exposed to ambient air while they were transferred to the reactor attachment for further treatment.

Binding energies (BE's) for samples containing alumina and ceria were referenced to Al2p at 74.5 eV and O1s at 529.0 eV, respectively. BE's of Pd⁰ and PdO in reference materials were referred to the Fermi edge of Pd and Cls at 284.6 eV, respectively.

XRD patterns were recorded on a Phillips X-ray generator with a Debye-Scherrer camera. CuK α X-rays (λ = 1.54178 Å) were used as the X-ray source. The recorded film was step-scanned with a microdensitometer. Particle diameters of Pd and ceria were estimated by the Scherrer relationship,

$$
t = 0.94\lambda/B\,\cos\,\theta,\qquad\qquad(1)
$$

where t is the particle diameter (A) , λ is the wavelength of CuK α radiation, θ is the Bragg angle, and \hat{B} is defined by

FIG. 1. Ce3d XPS spectra. (a) CeAl₂O₃; (b) CeO₂.

$$
B^2 = B_{\rm m}^2 - B_{\rm s}^2, \tag{2}
$$

where B_m is the measured line broadening for the sample and B_s is the instrumental line broadening measured using an α -Al₂O₃ standard.

3. XPS ANALYSIS

XPS spectra of cerium compounds are known to exhibit rather complex features due to hybridization with ligand orbitals and fractional occupancy of the valence $4f$ orbitals (13-16). The Ce3d XPS spectra of CeO₂ and 7 wt% CeAlO₃/Al₂O₃ are shown in Fig. 1. The complex spectrum of $CeO₂$ can be resolved into eight components by least-squares fitting with the assignment of each component defined in Fig. 1 (v) 's represent the Ce3d5/2 contributions and u 's represent the Ce3d3/2 contributions). The theoretical basis for all the components has been reported in the literature $(13, 15-16)$. The $u^{\prime\prime}$ peak, which arises from a transition of the $4f^0$ final state from the $4f^0$ initial state, has been used as a quantitative measure of the amount of Ce^{4+} (12). The u''' peak is absent from the Ce3d spectrum of CeAlO₃. The absence of the $u^{\prime\prime\prime}$ peak of the Ce3d spectrum of CeAlO₃, compared to that of $CeO₂$, is interpreted as the lack of the $4f^0$ configuration in the formal Ce³⁺ species.

It has been suggested that the $Ce3d$ spec-

FIG. 2. Composite Ce3d spectra.

trum from partially oxidized Ce can be approximated as a linear combination of spectra recorded from the oxides (17). Assuming a uniform mixture of Ce^{4+} and Ce^{3+} , the relative intensity of $u^{\prime\prime\prime}$ in the Ce3d region $(Ce3d5/2$ and $Ce3d3/2)$ can be used to describe quantitatively the chemical state of Ce. Other peaks are also displayed to demonstrate the basis employed for estimating the total areas in the Ce3d region. However, to obtain a consistent estimate of the spectral background (nonlinear Shirley background), a small contribution of $v^{\prime\prime\prime}$ is included in the Ce3d5/2 spectrum for $CeAlO₃$ even in the absence of the corresponding $u^{\prime\prime\prime}$ in the Ce3d3/2 region. This incorporation of the v''' peak should not influence the total area in the Ce3d region. Thus, it should be valid to utilize the percentage $u^{\prime\prime\prime}$ as a chemical identification for the amount of Ce^{4+} in the sample.

To translate the percentage $u^{\prime\prime\prime}$ in the Ce3d region into percentage of Ce^{4+} , the following scheme was employed. A series of composite Ce3d spectra was synthesized by superimposing the spectra of $CeO₂$ and $CeAlO₃$ (Fig. 1) at various proportions with normalized peak areas. A plot of percentage $u^{\prime\prime\prime}$ versus percentage CeO₂ (or 100%) $Ce⁴⁺$ for the composite spectra is shown in Fig. 2. The dashed line in Fig. 2 is obtained by a least-squares fit of the data points from the composite spectra through the origin,

whereas the solid Iine is a direct connection between end points derived from $CeO₂$ and $CeAlO₃$. This scheme is believed to provide a reasonable estimate for the percentages of $CeO₂$ and $Ce³⁺$ in the sample. The scatter of the points in Fig. 2 provides a measure for the accuracy of the spectra representatives. The relative error resulting from such a scheme is accordingly expected to be in the range of 10%.

4. RESULTS

4.1. XPS and XRD Results

4.1.1. Pd/Al_2O_3 and Pd/CeO_2 . XPS results of clean Pd foil, PdO, Pd/Al_2O_3 , and $Pd/CeO₂$ are summarized in Table 1. The Pd $3d5/2$ BE's obtained for Pd⁰ and PdO are in good agreement with published results $(18-20)$ and are used to identify the chemical states of Pd on catalyst samples.

After calcination at 800°C, Pd on alumina at 1.2 and 6.8 wt% yields a Pd $3d5/2$ BE of \approx 337.0 eV, which corresponds to that of PdO within experimental error $(\pm 0.15 \text{ eV})$. Reduction of the sample containing 6.8 wt% Pd at 500°C produces Pd⁰ (BE = 334.9) eV). After reduction in $H₂$ at 920°C, followed by exposure to air at room temperature, XPS indicates that no substantial reoxidation of Pd⁰ occurs during exposure to ambient air,

A similar study was conducted on 0.6 wt% $Pd/CeO₂$. This sample has a Pd loading comparable to that of 6.8% Pd/Al₂O₃ on the basis of the amount of Pd per square meter surface area of the support. As in the case of Pd on alumina, calcination of 0.6 wt% Pd on $CeO₂$ at 800°C produces a Pd $3d5/2$ BE of 336.9 eV, which is the BE of PdO (see Table 1). Reduction of the sample in situ at 500 $^{\circ}$ C results in formation of Pd 0 on ceria ($Pd3d5/2 = 335.1$ eV), as found in the case of Pd on alumina. After a more severe reduction at 920°C, followed by exposure to ambient air, Pd yields the Pd3d 5/2 BE of PdO (337.0 eV).

Thus, Pd reduced in H_2 at 920 $^{\circ}$ C and then exposed to ambient air produces PdO on

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Sample	Treatment history	BE (eV) $Pd3d5/2a$	Assignment	
Pd foil	Sputtered clean	334.9		
PdO	As received	336.8		
1.2% Pd/Al_2O_3	800°C calcined	337.0	PdO	
6.8% Pd/Al_2O_3	1. 800° C calcined	337.1	PdO	
	2.500° C reduced	334.9	Pd ⁰	
	3. 920° C reduced, then exposed to air	335.0	Pd ⁰	
0.6% Pd/CeO ₂	1. 800° C calcined	336.9	PdO	
	2.500° C reduced	335.1	Pd ⁰	
	3. 920°C reduced, then exposed to air	337.0	PdO	

XPS Data of Pd Foil, PdO, Pd/Al_2O_3 , and Pd/CeO_2

^a BE references are defined in the text.

ceria, but Pd metal on alumina. This difference suggests that ceria promotes the oxidation of Pd in air and thus confirms a suggestion reported in the literature (23).

4.1.2. $Pd - CeO_2/Al_2O_3$. Pd3d XPS spectra of 4.5 wt% Pd on alumina containing 18.4 wt% $CeO₂$ are shown in Fig. 3. After calcination at 8OO"C, the supported Pd is

FIG. 3. XPS spectra of Pd-CeO₂/Al₂O₃ catalysts containing 4.5% Pd and 18.4% CeO₂. (a) Calcined at 800°C; (b) reduced at 92O"C, exposed to air; (c) sample (b) reduced in situ at 500°C.

present mainly as PdO (Pd $3d5/2 = 337.0$ eV, Fig. 3a). Reduction at 920°C followed by exposure to air results in two different Pd species (Fig. 3b). The first species at 335.8 eV corresponds to a state between PdO and Pd 0 , while the second peak at a higher BE is probably attributable to Pd with chemisorbed oxygen (18) .

To explore the nature of the Pd species at 335.8 eV, the sample was reduced at 500°C (see Fig. 3 c). This reduction should reverse any surface oxidation which may have occurred during exposure to ambient air. The sample, reduced in situ at 500° C, gives a Pd $3d5/2$ BE of 334.8 eV, the BE of Pd 0 . A reduction at 500°C of a sample calcined at 800°C gives the same metallic Pd state $(Pd3d5/2 = 335.0 \text{ eV})$ (Table 2). Since reduction of both the calcined and prereduced samples leads to the formation of $Pd⁰$, the presence of the Pd species at 335.8 eV on the 920°C prereduced sample must be due to oxidation of Pd^0 on CeO_2/Al_2O_3 in ambient air. Compared to Pd supported on Al_2O_3 , where no significant oxidation of Pd⁰ is seen after exposure to ambient air, ceria on alumina apparently promotes the Pd oxidation. As mentioned above, a similar result has been noted for $Pd/CeO₂$ in the absence of alumina, where Pd is completely oxidized to PdO in ambient air.

TABLE 2

XPS Data for $Pd - CeO_2/Al_2O_3$

" Numbers in parentheses represent percentage of $CeO₂(Ce⁴⁺)$ in the Ce3d spectra, estimated on the basis of the dashed line in Fig. 2.

 $\frac{b}{A}$ denotes that samples have been exposed to air at room temperature after the treatment.

c Principal Pd3d5/2 peak.

Changes in the Ce chemistry, as measured by XPS analysis, are given in Table 2 and Fig. 4. In a previous study (12) , we have noted that a ceria-alumina interaction results in a highly stable dispersed ceria in the Ce(II1) state. The presence of this Ce(III) species, which is stable in air even at 800°C, lowers the total percentage $u^{\prime\prime\prime}$ in the Ce3d spectra and accounts for the fact that the $Ce⁴⁺$ contribution is always less than 100% as listed in Table 2. After calcination at 800°C, the percentages of the $u^{\prime\prime\prime}$ peaks amount to 9.3, 10.1, and 10.3%, for the samples containing 0, 4.5, and 9.2 wt% Pd, respectively. These percentages, corresponding to 65, 70, and 72% of Ce^{4+} (CeO₂), respectively, are constant within experimental error $(\pm 10\%)$. Thus, according to XPS analysis, Pd does not appear to modify the chemistry upon calcination of $CeO₂$ on alumina.

After reduction at 92O"C, followed by exposure to ambient air, the amount of Ce present as Ce⁴⁺ is found to increase with Pd loading (Figs. 4b-4d). The existence of $Ce⁴⁺$ is deemed to be the result of surface oxidation of $CeAlO₃$ to $CeO₂$ in ambient air in the presence of Pd, on the basis of the following observations. Reduction in situ at 500°C of the sample prereduced at 920°C results in the absence of the $u^{\prime\prime\prime}$ peak (Fig. 4e), which is characteristic for the total conversion of surface $CeO₂$ to $CeAlO₃$. The complete conversion to bulk $CeAlO₃$ on alumina from $CeO₂/Al₂O₃$ after reduction at 920° C, which has been confirmed by XRD (Fig. 5b and Table 3), is the general result of ceria reduction in the presence of Pd at high temperatures (\approx 920°C) and is discussed below.

This finding is supported by XPS data obtained after direct reduction at 500°C (Table 2). For 4.5 and 9.2% Pd on 18% CeO₂/ Al_2O_3 , the percentage $u^{\prime\prime\prime}$ remains essentially at the same value measured after calcination at 800°C and corresponds to $\approx 70\%$ $Ce⁴⁺$. The unchanged percentage of u''' indicates that reduction at 500°C is not sufficient to form $CeAlO₃$. Analysis by XRD of these samples reduced in situ at 500°C re-

FIG. 4. XPS spectra of Pd-CeO₂/Al₂O₃. (a) 4.5% Pd and 18.4% CeO₂, calcined at 800°C; (b) 0.9% Pd and 18.7% CeOz, reduced at 920°C; (c) 4.5% Pd and 18.4% CeO₂, reduced at 920°C; (d) 9.2% Pd and 16.2% CeO₂, reduced at 920°C; (e) reduction of sample (c) in situ at 500°C.

veals that Pd is present as $Pd⁰$ having a particle size of \simeq 15 nm, and Ce is in the form of CeOz. Both XPS and XRD data lead to the conclusion that reduction at 500°C does not convert $CeO₂/Al₂O₃$ to CeAlO₃ for samples within the Pd concentration range used.

FIG. 5. X-ray powder diffraction of $CeO₂/Al₂O₃$ containing 9.2% Pd on 16.2% CeO₂/Al₂O₃. (a) Calcined at 800°C; (b) sample (a) reduced at 920°C. (\triangle) γ -Al₂O₃; (\bullet) CeO₂; (\circlearrowright) CeAlO₃; (\diamondsuit) Pd⁰.

Without Pd, even reduction at temperatures as high as 920°C for 2 h did not complete conversion to CeAlO₃ in the 16.6% $CeO₂/Al₂O₃$ sample (Table 2 and Fig. 6b). This result indicates that both high temperature and the presence of Pd are required for the total conversion of $CeO₂$ into $CeAlO₃$ under the conditions used. It follows from analyses by XRD (Table 3) that Pd and Ce on the reduced sample are present as Pd^0 and $CeAlO₃$, respectively,

TABLE 3 X-ray Powder Diffraction for CeO₂/Al₂O₃ Containing Pd

	Treatment history	Particle size (nm)		
Sample		CeO ₂	CeAlO ₃	Pd
16.2% CeO ₂ /Al ₂ O ₃ ,	800°C calcined	8.2		
9.2% Pd doped ^a	920°C reduced/ A^a	---	25.2	25 Z

4 Sample has been exposed to air at room temperature after the treatment.

FIG. 6. XPS spectra of 16.6% CeO₂/Al₂O₃. (a) Calcined at 800°C; (b) reduced at 920°C.

and both species exist as small particles $(\simeq 25$ nm).

CeAlO₃, obtained by reduction of 18% $CeO₂/Al₂O₃$ at 920°C, is reoxidized to $CeO₂$ in ambient air (compare samples II and III under conditions (3a) and (3b) in Table 2). The oxidation is induced by Pd and does not occur without the metal (see sample I in Table 2). Meanwhile, Pd itself is partially oxidized, as noted previously. This result is based on XPS analysis. On the other hand, XRD gives no indication of any oxidation of either $CeAlO₃$ or Pd. The chemical state measured by XPS after oxidation at room temperature is therefore attributed to poorly crystallized $CeO₂$ on the alumina surface.

4.1.3. Pd -CeAlO₃/Al₂O₃. The results reported above are confirmed further by the use of cerium aluminate on alumina as a support for Pd. Data from XPS measurements of 10% CeAlO₃ on Al₂O₃ are summarized in Table 4. After 500°C calcination of a sample without Pd, virtually no change of $u^{\prime\prime\prime}$ in the Ce3d region is detected (within 10% error). However, when Pd is present in the sample, calcination at 500°C results in significant oxidation of $CeAlO₃$ to $Ce⁴⁺$, evident from a substantial increase in $u^{\prime\prime\prime}$. The extent of oxidation is the same (65%) for samples doped with 5 and 10 wt% Pd. Moreover, in both cases, Pd is present as PdO (Pd3*d5/2* BE of \simeq 336.8 \pm 0.2 eV). Reduction at 500°C of the calcined sample containing 5 wt% Pd restores the CeAlO₃ phase only partially $(4.7\% \; u^{\prime\prime\prime})$ or 35% Ce⁴⁺ in the sample), while Pd is reduced to its metallic state. The incomplete conversion of $CeO₂$ to $CeAlO₃$ after the reduction corroborates the conclusion that reduction of bulk $CeO₂$, even in the presence of Pd, requires a temperature above 500°C.

The bulk structure of 10% CeAlO₃ on Al_2O_3 was also examined by XRD. Results are shown in Figs. 7 and 8. Diffraction lines of samples without Pd, either fresh or calcined at 5OO"C, are attributable to CeAlO₃ and γ -Al₂O₃. However, as shown in Fig. 8, samples doped with 1 or 5 wt% Pd $(Pd/CeO₂)$ molar ratios are 0.16 and 0.81, respectively) and calcined at 500°C contain, in addition, $CeO₂$. As the Pd loading is increased to 10 wt% Pd (atomic Pd/Ce = 1.6), the diffraction lines of $CeAlO₃$ disappear al-

TABLE 4 XPS Data of 10% CeAlO₂/ALO₂ Containing Pd

Sample	Treatment history	$\%u''$	BE (eV) Pd3d5/2	
Undoped	1. As prepared ^b	$3.4(23)^a$		
	2. 500°C calcined	4.4(32)		
5% Pd doped	1. 500°C calcined	9.3(65)	337.0	
	2. 500°C in situ reduced	4,7(35)	335.0	
10% Pd doped	1. 500°C calcined	9.4(66)	336.7	

 α Numbers in parentheses represent percentage of Ce⁴⁺ in the sample, as estimated on the basis of the correlation curve in Fig. 2.

b Prepared by reduction at 1000°C of 10% CeO₂/Al₂O₃ for 80 h.

FIG. 7. X-ray powder diffraction of 10% CeAlO₃/ Al_2O_3 . (a) As prepared; (b) sample (a) calcined at 500°C. (O) CeAlO₃; (\triangle) γ -Al₂O₃.

together (Fig. 8c). It appears therefore that complete oxidation of bulk $CeAlO₃$ requires an amount of Pd which is not less than the amount of Ce in the sample.

No diffraction lines associated with Pd are detected in any of the oxidized samples (Figs. 8a-8c). An explanation is given by the fact that Pd is present as dispersed PdO (less than \approx 5 nm) on alumina. As expected, reduction of the same sample at 920°C restores the $CeAlO₃$ phase completely (Fig. 8d), while Pd becomes detectable as Pd⁰ with a particle size of $\simeq 35$ nm (Table 5).

FIG. 8. X-ray powder diffraction of Pd on 10% CeAl₂O₃/Al₂O₃. (a) 1% Pd, calcined at 500°C; (b) 5% Pd, calcined at 500°C; (c) 10% Pd, calcined at 500°C; (d) 10% Pd, reduced at 920°C. (\triangle) γ -Al₂O₃; (\bullet) CeO₂; (O) CeAlO₃; (\diamond) Pd^o.

It is apparent from these results that Pd assists in the oxidation of CeAlO₃ to $CeO₂$. Unlike the oxidation of $CeAlO₃$ in the presence of Pd at room temperature, where only surface oxidation is evident, calcina-

TABLE 5

Sample	Treatment history	Particle size (nm)		
		CeO ₂	CeAlO ₃	Pd
Undoped	As prepared		22.2	
	500°C calcined		19.1	
1% Pd doped	500°C calcined	18.8	15.5	
5% Pd doped	500°C calcined	19.6	5.5	
10% Pd doped	500°C calcined	22.0		
10% Pd doped	920°C reduced/ A^a		18.5	35.7

X-Ray Powder Diffraction Data for 10% CeAlO₃/Al₂O₃

a Sample has been exposed to air at room temperature after the treatment.

FIG. 9. Propane oxidation on 10 wt% Pd/ γ -Al₂O₃. Feed gas: 1000 ppm C_3H_8 and 2.0% O_2 . (\circlearrowright) Undoped; \bullet) doped with 10 wt% CeO₂.

tion at 500°C results in bulk oxidation of CeAlO₃ to $CeO₂$. This conclusion is based on both XPS and XRD.

4.2. Propane Oxidation over $Pd-CeO₂/Al₂O₃$ Catalysts

Propane oxidation by oxygen was used in this study as a model reaction to probe catalytic additive effects of ceria on Pd/Al_2O_3 . The reaction mixture at the catalyst inlet consists of 1000 ppm C_3H_8 and 2% O_2 in N₂; i.e., the oxygen concentration is four times that required for a complete oxidation of propane to $CO₂$ and H₂O. Typical reaction curves of propane oxidation on 10% Pd/

 Al_2O_3 with and without 10% CeO₂ added are given in Fig. 9. The temperature at 50% propane conversion, T_{50} , was chosen as an activity index. As shown in Fig. 9, addition of ceria to 10 wt% Pd on Al_2O_3 increases T_{50} from 288 to 343°C; i.e., it lowers the catalyst activity. Thus, the presence of ceria can deactivate Pd/AI_2O_3 catalysts to some extent.

Reaction curves measured with stoichiometric feed gas $(C_3H_8: Q_2 = 1:5)$ are shown in Fig. 10. Again, the added 10 wt% ceria lowers the catalyst activity. The effect, however, is smaller at the stoichiometric oxygen concentration, characterized by an increase in T_{50} from 304 to 329°C.

The influence of oxygen concentration on the ceria effect is illustrated further by results shown in Fig. 11. In this case reaction isotherms were measured at 350°C and oxygen levels from 0.25 to 4%. Clearly, in the absence of ceria, propane oxidation over 10% Pd/Al₂O₃ is unaffected by the feed gas composition in the range given. On the other hand, in the presence of ceria, an abrupt decrease in conversion occurs when conditions are changed from stoichiometric to oxidizing. Above 2% oxygen no further change in activity takes place. It should also be noted that at 0.25% oxygen the rate of propane oxidation over 10% Pd/Al₂O₃ is the same with and without ceria. Only

FIG. 10. Propane oxidation on 10 wt% Pd/ γ -Al₂O₃. Feed gas: 1000 ppm C_3H_8 and 0.5% O₂. (O) Undoped; (\bullet) doped with 10 wt% CeO₂.

FIG. 11. Propane oxidation on 10 wt% Pd/y-Al₂O₃. $C₃H₈$ concentration in feed gas: 1000 ppm. Reaction temperature: 350° C. (O) Undoped; (\bullet) doped with 10 wt% $CeO₂$.

when the oxygen concentration exceeds the stoichiometric ratio does the addition of ceria to Pd/Al_2O_3 cause catalyst deactivation. The kinetic data, together with results derived from XPS and XRD, indicate that the presence of ceria modifies the Pd chemistry under oxidizing conditions.

5. DISCUSSION

The experimental results presented in this paper can be summarized as follows:

1. With or without alumina, ceria promotes the oxidation of Pd to PdO. As a result, addition of $CeO₂$ to $Pd/Al₂O₃$ retards the catalytic oxidation rate of propane over palladium for reactant mixtures which exceed the stoichiometric O_2/C_3H_8 ratio, in which palladium is presumably in its oxidized state.

2. Upon reduction at high temperatures, palladium assists in the formation of bulk CeAlO₃ from CeO₂/Al₂O₃. Also, Pd catalyzes bulk oxidation of $CeAlO₃$ at elevated temperatures.

3. Palladium assists in the surface oxidation of $CeAlO₃$ in ambient air, whereas surface Pd is partially oxidized to a state between Pd^0 and PdO .

On the basis of these observations, it is apparent that cerium oxides and palladium are subject to mutual interaction. Such an interaction has been proposed by Sass *et al*. (23, 26) on the basis of EPR and reaction activity measurements in which an active $O₂$ species has been identified.

According to the XPS data in this study, surface oxidation of $CeAlO₃$ by Pd may also entail an intermediate species containing $Pd+O₇$. Coordinately unsaturated CeAlO₃ adsorbs oxygen in air to form $O₂$ species (8), which may be stabilized by forming a surface species with palladium. Thus, a tentative model is derived to explain the experimental observations. The model is based on the structure

In this proposed structure of the oxidized surface species, Pd is in a state between Pd^0 and PdO, whereas cerium is in its tetravalent state. This surface complex can be reduced at mild temperatures to form Pd⁰ and $CeAlO₃$, while oxidation results in splitting of the $O₂$ species to form bulk PdO and $CeO₂$. It appears that palladium plays an important role in both formation and oxidation of $CeAlO₃$. Adsorption of oxygen results in the formation of $O₇$ (8, 26, 27) that is stabilized in the coordination sphere of the palladium and cerium ions (22, 23) and leads to the reversible formation of CeAlO₃ from CeO₂/Al₂O₃.

Mutual influences between Pd and ceria are also reflected in the propane oxidation. Strong dependence of the oxidation rate of propane on oxygen concentration over Pd/ $A₁$, containing ceria is interpreted as surface chemical changes of Pd by ceria under oxidizing conditions. As shown previously, under oxidizing conditions, Pd is converted to PdO in the presence of ceria. The formation of PdO is accompanied by a lower propane oxidation rate, a result which is consistent with conclusions published earlier from this laboratory (2, 25). Therefore, from a practical standpoint in automotive catalysis, the air/fuel ratio should be adjusted near the stoichiometric ratio when Pd and ceria are both present. This allows a more efficient use of Pd without losing other important functions that ceria can provide, such as stabilization of γ -Al₂O₃, dispersion of Pt and Rh, and oxygen storage.

6. CONCLUDING REMARKS

In summary, it can be stated that a complex interaction among ceria, palladium, and alumina clearly influences the reversible reaction

$$
2CeO2 + Al2O3 + H2 \xleftrightarrow{\frac{H_2}{O_2}}
$$

2CeAlO₃ + H₂O

This interaction is detected after reduction at 92O"C, when the formation of bulk aluminate is catalyzed in the presence of Pd; during the reverse reaction, the oxidation of bulk aluminate at 500°C is also catalyzed by Pd. A distinct modification of Pd in ambient air was demonstrated by an oxidation state between Pd^0 and PdO .

7. REFERENCES

- 1. Gandhi, H. S., Piken, A. G., Shelef, M.. and Delosh, R. G., SAE Paper No. 760201, Warrendale, PA (1976).
- 2. Yu-Yao, Y. F., and Kummer, J. T., J. Catal. 106, 307 (1987).
- 3. Yao, H. C., and Yu-Yao, Y. F., J. Catal. 86, 254 (1984).
- 4. Yao, H. C., Gandhi, H. S., and Shelef, M., in "Metal-Support and Metal-Additive Effects in Catalysis" (B. Imelik, Ed.). Elsevier, Amsterdam, 1982.
- 5. Su, E. C., and Rothschild, W. G., J. Catal. 99, 506 (1986).
- 6. Su, E. C., Montreuil, C. N., and Rothschild, W. G., Appl. Catal. 17, 75 (1985).
- 7. Rosynek, M. P., Catal. Rev. Sci. Eng. 16, 111 (1977).
- 8. Kaufherr, N., Mendelovici, L., and Steinberg, M., J. Less Common Met. 107, 281 (1985).
- Yamaguchi, T., Ikeda, N., Hattori, H., and Tanabe, K., J. Catal. 67, 324 (1981).
- 10. Mizuno, M., Berjoan, R., Coutures, J. P., and Feox, M., Yagyo-Kyokai-Shi 83, 50 (1975).
- 11. Geller, S., and Raccah, P. M., *Phys. Rev. B* 2, 1167 (1970).
- 12. Shyu, J. Z., Weber, W. H., and Gandhi, H. S., J. Phys. Chem., in press.
- 13. Fujimori, A., J. *Magn. Magn. Mater*. **47, 48,** 243 (1985).
- 14. Allen, J. W., J. Magn. Magn. Mater., 168 (1985).
- 15. Fujimori, A., Phys. Reu. B 28, 2281 (1983).
- 16. Fujimori, A., *Phys. Rev. B* 27, 3992 (1983).
- 17. Platau, A., Ph.D. thesis, Linkoping University, Sweden, 1982.
- $18.$ Kim, K. S., Gossman, A. F., and Winograd, N., Anal. Chem. 46, 197 (1974).
- 19. Bozon-Verduraz, F., Omar, A., Ecsad, J., and Pontvianne, B., J. Catal. 53, 126 (1978).
- 20. Kohini, S., Appl. Surf. Sci. 25, 81 (1986).
- 21. Summer, J. C., and Ausen, S. A., J. Catal. 58. 131 (1979).
- 22. Mendelovici, L., Tzehoval, H., and Steinberg, M., Appl. Surf. Sci. 17, 175 (1983).
- 23. Sass, A. S., Kuznetsov, A. V., Shvets, V. A., Savel'eva, G. A., Popova, N. M., and Kazanskii, V. B., Kinet. Catal. 26, 1217 (1985).
- 24. Yu-Yao, Y. F., private communication.
- 25. Yu-Yao, Y. F., Ind. Eng. Prod. Res. Dev. 19, 29 (1980).
- 26. Sass, A. S., Shvets, V. A., Savel'eva, G. A., Popova, N. M., and Kazanskii, V. B., Kinet. Catal. 27, 799 (1986).
- 27. Shubin, V. E., Shvets, V. A., Savel'eva, G. A., Popova. N. M., and Kazanskii, V. B., Kinet. Catal. 23, 982 (1982).